



# A green, efficient reductive N-formylation of nitro compounds catalyzed by metal-free graphitic carbon nitride supported on activated carbon

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## ABSTRACT

Metal-free graphitic carbon nitride supported on activated carbon was fabricated via a simple pyrolysis for one-pot reductive N-formylation of nitro compounds with formic acid and sodium formate was employed as promoter. Under the conditions, this transformation was successfully achieved without any solvent. The support activated carbon and pyrolysis atmosphere had important influence on catalytic behavior of catalyst. SEM, TEM, XRD, XPS, EPR, FT-IR, Raman spectrum and N<sub>2</sub> adsorption/desorption characterizations revealed that air pyrolysis enabled g-C<sub>3</sub>N<sub>4</sub> to generate more carbon defects and the support AC effectively dispersed g-C<sub>3</sub>N<sub>4</sub> to expose more active sites. Using our procedure, a broad set of nitro compounds was converted to their corresponding formamides with various functional group tolerances. The catalyst could be recycled several times without marked loss of activity. In short, we provided an efficient and sustainable protocol for the expedient synthesis of formamides from nitro compounds.

## 1. Introduction

The amide bond is pervasive in nature and one of the most important functional groups. A comprehensive survey exhibited that more than 25% of known drugs contained an amide group [1]. Among various amides, formamides have been extensively applied in pharmaceuticals, fragrances, agrochemicals, dyes and polymers [2,3]. Moreover, formamides serve as industrial solvents [4] and catalyst [5]. Thus, the production of formamide has attracted considerable attention. In the past decades, it was extensively studied to synthesize N-formamides by the condensation of amines with formylating reagents, such as methanol [6,7], formic acid [8–12] and (para)-formaldehyde [13]. However, this route suffers from the drawbacks of the production of massive wastes and unsatisfactory atom-efficiency. Therefore, it is desirable to develop an economical, environmentally friendly and greener process in organic chemistry and industry.

Recently, a novel protocol, the one-pot direct reductive N-formylation of nitro compounds to N-formamides, was developed [14]. The successive multistep transformation involves hydrogen production, transfer hydrogenation of nitro compounds and the condensation of amines with formylating reagents. Compared with N-formylations of amines to N-formamides, this synthetic route avoids hydrogenation process of nitro compounds as well as associated separation and

purification steps. Obviously, formylating reagents have played a key role in the transformation. Formic acid (FA), as a renewable material, is an easy-to-handle liquid hydrogen donor with 4.4 wt% hydrogen content, and it can also be used as the formylating reagents. So, FA is an excellent alternative as hydrogen and formylating source for this transformation. To date, the direct reductive N-formylations of nitro compounds with formic acid to N-formamides were usually achieved in the presence of metal catalysts including noble metal (e.g. Pd [15,16], Au [17], Rh [18], etc.) and non-noble metal (Co [19,20] and Zn [21,22]). These metal catalytic systems exhibit considerable advances, whereas there are different levels of drawbacks. Firstly, the reagent FA generates acidic environment, so the leaching of metal is almost inevitable for these metal catalysts, resulting in the decline of catalytic performance of catalyst as well as metal pollution of product. Moreover, the scarcity and high cost of metal catalysts (especially noble metal catalysts) impede their practical applications. Therefore, there exists growing incentive to develop an inexpensive and efficient catalyst for the reductive N-formylations of nitro compounds to formamides. If we can design a kind of metal-free catalyst for the reductive N-formylations of nitro compounds with FA, it would avoid the use of noble metal and the leaching of metal catalyst fundamentally. Based on the aim, this study is committed to exploring a metal-free catalyst and eco-friendly protocol for the reductive N-formylations of nitro compounds with FA to formamides. To the

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best of our knowledge, there are no reports of non-metallic catalysts for this transformation.

Carbon materials, such as carbon nanotubes [23,24], graphene [25], carbon nitride [26], have attracted extensive interests in many fields. Among these, carbon nitride is widely studied in the catalysis field due to unique structure, electronic properties, low cost and non-pollution. For instance, g-C<sub>3</sub>N<sub>4</sub> has been applied in photocatalysis [27,28], environmental protection [29–31] and electrochemistry [32]. And beyond that, g-C<sub>3</sub>N<sub>4</sub> was also used as heterogeneous catalyst in organic reaction (e.g Friedel-Crafts reaction [33], Knoevenagel condensation [34] and acetylene hydrochlorination [35]).

Herein, we developed an effective g-C<sub>3</sub>N<sub>4</sub> supported on activated carbon (AC) as metal-free catalyst for the one-pot reductive N-formylations of nitro compounds to formamides. And, formic acid-sodium formate (SF) system was employed innovatively as hydrogen source to improve the reaction efficiency. The relationship between catalyst property and catalytic performance of g-C<sub>3</sub>N<sub>4</sub> supported on activated carbon was discussed and a green and efficient protocol of N-formylations of nitro compounds to formamides was established.

## 2. Experimental section

### 2.1. Materials

Activated carbon was obtained from Xilong Scientific Co., Ltd. Other chemicals were purchased from Sinopharm Chemical Reagent Co., Ltd. and Shanghai Macklin Biochemical Co., Ltd. Beyond that, all the reagents were of analytical grade or higher and were used without further purification.

### 2.2. Catalyst preparations

Typically, Dicyandiamide (DCD, 6.7 g) were dissolved in deionized water; activated carbon powder (AC, 6.7 g) was added to the above solution. Then, the suspension was stirred at 50 °C until the bulk water evaporated completely, and the obtained solid was further dried at 120 °C for 1 h. Subsequently, the solid mixture was transferred into a covered ceramic crucible (semi-closed state). Then the crucible filled with catalyst precursor was calcined at 550 °C for 1.5 h at a ramp rate of 5 °C/min in static air and N<sub>2</sub> flow, respectively. After naturally cooling down to room temperature, the desired products were obtained, which was named g-C<sub>3</sub>N<sub>4</sub> @AC-A and g-C<sub>3</sub>N<sub>4</sub> @AC-N, here A and N represented air and nitrogen atmosphere, respectively.

In addition, in order to study catalytic mechanism, pure g-C<sub>3</sub>N<sub>4</sub>-A and g-C<sub>3</sub>N<sub>4</sub>-N were prepared by the above method in the absence of AC.

### 2.3. Characterizations

Powder X-ray radiation diffraction (XRD) was recorded on a Rigaku Utima IV (Cu K $\alpha$  radiation,  $\lambda = 0.154178$  nm). The textural properties of the as-prepared catalyst samples were collected on the ASAP 2460 instrument at 77 K; the specific surface area was calculated using the Brunauer-Emmett-Teller (BET) method; the pore volume and pore size distribution were obtained using the Barrett-Joyner-Halenda (BJH) method. The determination of elements of the catalysts samples was performed by X-ray Photoelectron Spectroscopy (XPS) (Thermo Fisher ESCALAB Xi+). Fourier Transform Infrared Measurement (FT-IR) was carried out using Nicolet iS50 spectrometer. The electron paramagnetic resonance spectra (ESR) of the catalyst samples were determined using Bruker EMXplus spectrometer. The Raman spectra were obtained on Thermo Fisher DXR2 spectrometer. A scanning electron microscope (SEM) (Hitachi S-4800) was used for the morphology and transmission electron microscopy imagines (TEM) were obtained on FEI talos F200X.

### 2.4. Typical procedure for the one-pot reductive N-formylation of nitro compounds to N-formamides

The one-pot reductive N-formylation of nitro compounds to N-formamides was carried out in a stainless steel teflon-lined autoclave reactor (50 mL). In a typical reaction procedure, nitro compounds (5 mmol), formic acid (40 mmol), sodium formate (10 mmol) and the catalyst (0.3 g) were added to the autoclave reactor. Before the reaction started, the autoclave was purged with argon gas and sealed under normal pressure. The mixture was vigorously agitated by a magnetic stirrer at 120 °C for a given period of time. After the completion of the reaction, the reactor was cooled to room temperature. Ethyl acetate was added (10 mL) to the reaction mixture and stirred at 60 °C for half an hour. Then filtration was conducted to separate the solid catalyst, and the obtain residue was washed by ethyl acetate to completely extract the organic compound. The ethyl acetate extract mixtures were collected together and analyzed by using Agilent GC-MS 7890 and Shimadzu GC-2010 Plus with a FID detector (Dodecane as a GC internal standard). The reaction products were confirmed by GC-MS as well as by comparing the retention times of standard substances in GC traces.

## 3. Results and discussion

### 3.1. Optimization of reaction conditions

The one-pot reductive formylation reaction of nitrobenzene and FA was selected as the model reaction to optimize the catalytic system and reaction conditions (Table 1). In the initial research, based on our study accumulation in N-doping carbon based transition metal catalyst [36–38], Co-N-C and Cu-N-C composite supported on AC were prepared for the formylation reaction. It was found that the metal badly leached from catalyst in acidic environment although protective structures (metal particle encapsulated in CNT and coated by carbon layer) were formed in these catalysts (seeing references 36–38). Associating with the fact that metal-free nitrogen-carbon composites possessed hydrogenation property [39,40], we attempted to prepare a g-C<sub>3</sub>N<sub>4</sub> supported on activated carbon without any metal by the pyrolysis process in nitrogen (g-C<sub>3</sub>N<sub>4</sub> @AC-N) for this transformation. And an amide yield of 28% was obtained, which demonstrated that metal-free nitrogen-carbon composite had encouraging potential (Entry 1, Table 1). The previous studies revealed that the introduction of HCOO<sup>-</sup> facilitated the dehydrogenation rather than dehydration and avoided the O-H cleavage step with high activation energy requirement, so the hydrogen production rate was higher in a mixture of FA and SF than FA-only [41,42]. From this, FA-SF mixed system was employed instead of FA to speed the formylation reaction of nitrobenzene. As expected, the introduction of SF distinctly stimulated the transformation (Entry 2, Table 1). Then the amount of SF was investigated, and the 4:1 molar ratio of FA to SF gave the best result (Entry 3, Table 1). Subsequently, the effect of solvents was also investigated; the desired product could be obtained in solvents. Nevertheless, the best yield was still achieved under solvent-free condition (Table S1).

Furthermore, a g-C<sub>3</sub>N<sub>4</sub> supported on activated carbon pyrolyzed in air was tested, and it exhibited higher catalytic activity compared to g-C<sub>3</sub>N<sub>4</sub> @AC-N (Entry 1 and 2, Table 2). This illustrated that pyrolysis

**Table 1**  
The effect of SF on the formylation reaction of nitrobenzene with FA a.

Entry	Amount of SF	Amide yields (%) <sup>b</sup>
1	HCOONa (0 mmol)	28
2	HCOONa (5 mmol)	40
3	HCOONa (10 mmol)	46
4	HCOONa (15 mmol)	43

<sup>a</sup>Nitrobenzene (5 mmol), FA(40 mmol), g-C<sub>3</sub>N<sub>4</sub> @AC-N (0.3 g), 120 °C, 4 h, N<sub>2</sub> atmosphere.

<sup>b</sup>GC Yields.

**Table 2**Reductive N-formylation of nitrobenzene with FA on various catalysts <sup>a</sup>.

		Cat.	HCOOH-HCOONa	1a	2a	3a	4a	5a	
Entry	Catalysts	Reaction conditions		Con. (%) <sup>b</sup>	Selec. (%) <sup>b</sup>				
					2a	3a	4a	5a	others
1	g-C <sub>3</sub> N <sub>4</sub> @AC-N	120 °C/4 h		47	0.3	0.2	n.d	98.2	1.3
2	g-C <sub>3</sub> N <sub>4</sub> @AC-A	120 °C/4 h		61	0.1	0.3	n.d	98.5	1.1
3	g-C <sub>3</sub> N <sub>4</sub> -N	120 °C/4 h		10	1.8	2.0	0.5	92.5	3.2
4	g-C <sub>3</sub> N <sub>4</sub> -A	120 °C/4 h		16	1.1	2.9	1.3	91.7	3.0
5	g-C <sub>3</sub> N <sub>4</sub> @AC-A	130 °C/10 h		99	n.d	0.6	0.2	99.0	0.2
6	—	120 °C/4 h		4	1.5	n.d	n.d	76.1	22.4

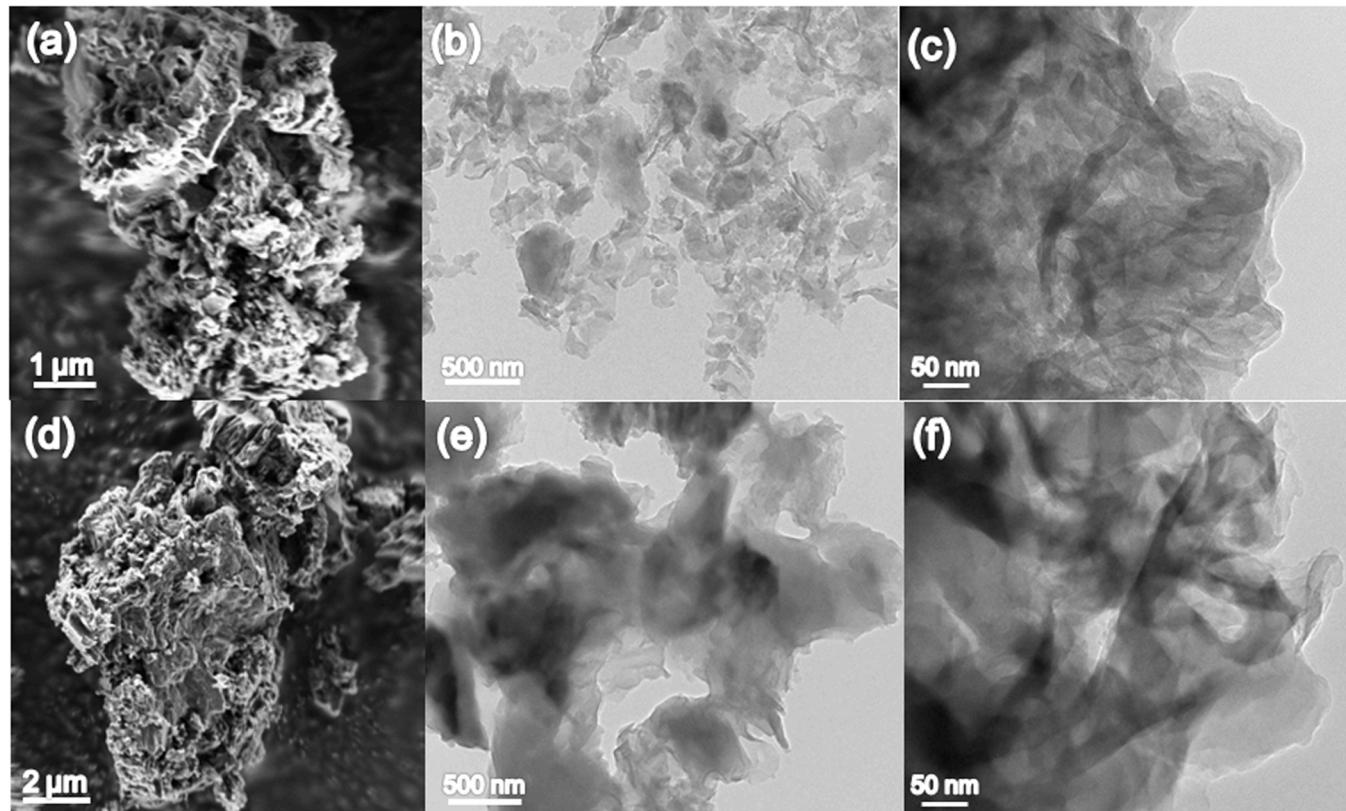
<sup>a</sup> Reaction conditions: nitrobenzene (5 mmol), FA (40 mmol), SF (10 mmol), catalyst (0.3 g), N<sub>2</sub> atmosphere.<sup>b</sup> GC results

atmosphere had important role on catalytic behavior of catalyst. The corresponding g-C<sub>3</sub>N<sub>4</sub>-N and g-C<sub>3</sub>N<sub>4</sub>-A samples without support were also prepared and examined, and similar results were obtained. The catalytic performance of g-C<sub>3</sub>N<sub>4</sub>-A was better than that of g-C<sub>3</sub>N<sub>4</sub>-N (Entry 3 and 4, Table 2). And, the activities of two pure g-C<sub>3</sub>N<sub>4</sub> samples were much lower compared with the corresponding supported, which manifested that the support AC had significant influence on catalytic performance. In order to completely achieve the transformation, we raised reaction temperature and prolonged reaction time, and a 98% yield of formamide was acquired (Entry 5, Table 2). Additionally, an experiment was also carried out in the absence of catalyst; only a small amount of formamide was obtained (Entry 6, Table 2). The blank

experiment proved the effectiveness of these metal-free nitrogen-carbon composites.

### 3.2. Structure characterization and catalytic mechanism of nitrogen-carbon composites

To understand the catalytic properties of nitrogen-carbon composites and reveal the catalytic mechanism involved, the morphology and microstructure of pure g-C<sub>3</sub>N<sub>4</sub> samples in different pyrolysis atmosphere were observed by SEM and TEM. It could be seen from SEM images in Fig. 1(a) and (d) that pure g-C<sub>3</sub>N<sub>4</sub> samples displayed bulk morphology of agglomerates with nano-and micro-pores on the surface. g-C<sub>3</sub>N<sub>4</sub>-A had



**Fig. 1.** The morphology and microstructure characterization of pure g-C<sub>3</sub>N<sub>4</sub> samples: (a) SEM image of g-C<sub>3</sub>N<sub>4</sub>-A, (b) (c) TEM images of g-C<sub>3</sub>N<sub>4</sub>-A; (d) SEM image of g-C<sub>3</sub>N<sub>4</sub>-N, (e) (f) TEM images of g-C<sub>3</sub>N<sub>4</sub>-N.

more pores and looser morphology than g-C<sub>3</sub>N<sub>4</sub>-N. TEM micrographs also supported it (seeing Fig. 1(b) and (e)). Moreover, thinner sheets and wrinkles with roughness or grain boundaries were presented in g-C<sub>3</sub>N<sub>4</sub>-A in Fig. 1(c) and (f), hereby creating more edges and defects which improved the performance of the catalyst.

Next, XRD was performed to characterize the crystalline structures of the catalysts. Fig. 2 showed the XRD patterns of various catalyst samples. For pure g-C<sub>3</sub>N<sub>4</sub>, two significant characteristic peaks of g-C<sub>3</sub>N<sub>4</sub> at around 13.5° and 27.5°, assigned to the (100) and (002) planes, were observed [43,44]. XRD patterns of the two supported g-C<sub>3</sub>N<sub>4</sub> samples only displayed two broad peaks, no characteristic peaks of g-C<sub>3</sub>N<sub>4</sub> were found. Combined with XRD pattern of AC, the peak centered at 43.2° could be attributed to the (101) planes of AC, whereas the peak centered at 23.9° should be a joint result of 27.5° peak of g-C<sub>3</sub>N<sub>4</sub> and 21.6° of AC support. The analyses demonstrated that g-C<sub>3</sub>N<sub>4</sub> was formed in the supported g-C<sub>3</sub>N<sub>4</sub> samples and well dispersed on the support surface, which was one of reason for why the activity of the supported g-C<sub>3</sub>N<sub>4</sub> samples were higher than that of pure g-C<sub>3</sub>N<sub>4</sub> samples. In-depth analyses showed that pure g-C<sub>3</sub>N<sub>4</sub> fired in an air atmosphere than in a N<sub>2</sub> atmosphere the (002) peak shifted to higher angles (from 27.44° to 27.78°), correspondingly interlayer distance decreased from 0.325 nm to 0.321 nm (Table S2). And, the intensity of diffraction peaks of g-C<sub>3</sub>N<sub>4</sub>-A was slightly stronger than that of g-C<sub>3</sub>N<sub>4</sub>-N demonstrating that the crystallite size increased, which seemed not to support the activity test results because the smaller crystallite size generally possessed higher catalytic activity. Thus, XPS was carried out to gain more details on the structure and composition of the as-prepared catalysts.

The full XPS survey spectra indicated the samples were mainly made up of C, N, and O elements (Fig. S1). Correspondingly, the atom ratios of carbon to nitrogen ( $R_{C:N}$ ) of g-C<sub>3</sub>N<sub>4</sub>-N and g-C<sub>3</sub>N<sub>4</sub>-A were calculated to be 0.89 and 0.84 (Table S3), respectively, which showed that greater carbon loss occurred in air atmosphere calcination. Previous work suggested that such variation of C/N ratio meant the generation of carbon defect sites [45–47]. Meanwhile, defect as catalytic site had been widely investigated and accepted in catalysis [48,49]. It was therefore reasonable to conjecture that there were more richly available carbon defects on the surface of g-C<sub>3</sub>N<sub>4</sub>-A prepared in this study than g-C<sub>3</sub>N<sub>4</sub>-N. To understand this proposed carbon defect formation, the resolutions of element spectrum peaks of g-C<sub>3</sub>N<sub>4</sub>-A and g-C<sub>3</sub>N<sub>4</sub>-N were carefully

conducted to analyze the difference of chemical state of elements. As shown in Fig. 2, XPS spectra of g-C<sub>3</sub>N<sub>4</sub>-A and g-C<sub>3</sub>N<sub>4</sub>-N could be deconvoluted into four peaks at 284.5, 286.1, 287.9 eV and 288.7 eV, which ascribed to adventitious carbon, the carbon in C-NH<sub>x</sub> groups, tertiary carbon C<sub>3</sub>N and =CNH<sub>2</sub> groups, denoted as C<sub>1</sub>, C<sub>2</sub>, C<sub>3</sub>, and C<sub>4</sub>, respectively [50,51], demonstrating that these two samples maintained a basic tri-s-triazine structure. Meanwhile, the C<sub>3</sub> ratio in the whole carbon decreased from 0.68 of g-C<sub>3</sub>N<sub>4</sub>-N to 0.65 of g-C<sub>3</sub>N<sub>4</sub>-A (Table S4), which suggested the missing of carbon moiety and formation of more carbon defects at the tertiary carbon sites [50]. Additionally, the previous studies indicated that the content of amino groups was positively related to the carbon defect at tertiary carbon and the ratio of C<sub>3</sub> to C<sub>4</sub> implied the changed concentration of amino groups to some extent [52–54]. In our case, g-C<sub>3</sub>N<sub>4</sub>-A showed the lower ratio of C<sub>3</sub>/C<sub>4</sub> compared with the counterpart (5.42 vs 7.56, Table S4), which represented a higher the content of amino groups, further manifesting the higher concentration of carbon defects in g-C<sub>3</sub>N<sub>4</sub>-A. The N 1 s spectra of the samples also could confirm this issue. Four main peaks at 398.5, 399.7, 400.9, and 404.0 eV, assigned to sp<sup>2</sup>-hybridized C=N-C structure (N<sub>1</sub>), tertiary nitrogen N-(C)<sub>3</sub> (N<sub>2</sub>), -NH<sub>x</sub> groups (N<sub>3</sub>) and π excitation effect in heptazine rings (N<sub>4</sub>), respectively, were identified in the N 1 s spectra (Fig. 2) [55,56]. The report pointed out that the ratio of N<sub>3</sub>/N<sub>2</sub> had a positive relation with the number of amino groups [57], while the higher content of amino groups signified more carbon defects, so g-C<sub>3</sub>N<sub>4</sub>-A with the bigger ratio value of N<sub>3</sub>/N<sub>2</sub> (0.83 vs 0.61) had higher content of carbon defects (Table S5) [53,57,58]. Note that the presence of amino groups generated hydrogen-bonding interaction between g-C<sub>3</sub>N<sub>4</sub> layers to result in the decrease of the distance between interlayer [58]. Therefore, g-C<sub>3</sub>N<sub>4</sub>-A containing larger number of amino groups exhibited the smaller interlayer distance, which corresponded with the XRD results. To further confirm carbon defects, EPR was used to detect the formation of surface defects.

Fig. 3a depicted ESR spectra of pure g-C<sub>3</sub>N<sub>4</sub>-N and g-C<sub>3</sub>N<sub>4</sub>-A. As observed, two samples exhibit a major ESR signal with g value of 2.004, ascribed to unpaired electrons on carbon atoms of the heptazine rings. Compared with g-C<sub>3</sub>N<sub>4</sub>-N, the ESR signal intensity of g-C<sub>3</sub>N<sub>4</sub>-A attenuated, which demonstrated the less of carbon content in its structure, further indicating the formation of carbon vacancies in g-C<sub>3</sub>N<sub>4</sub>-A samples [47,52,59]. Subsequently, the surface groups on samples were

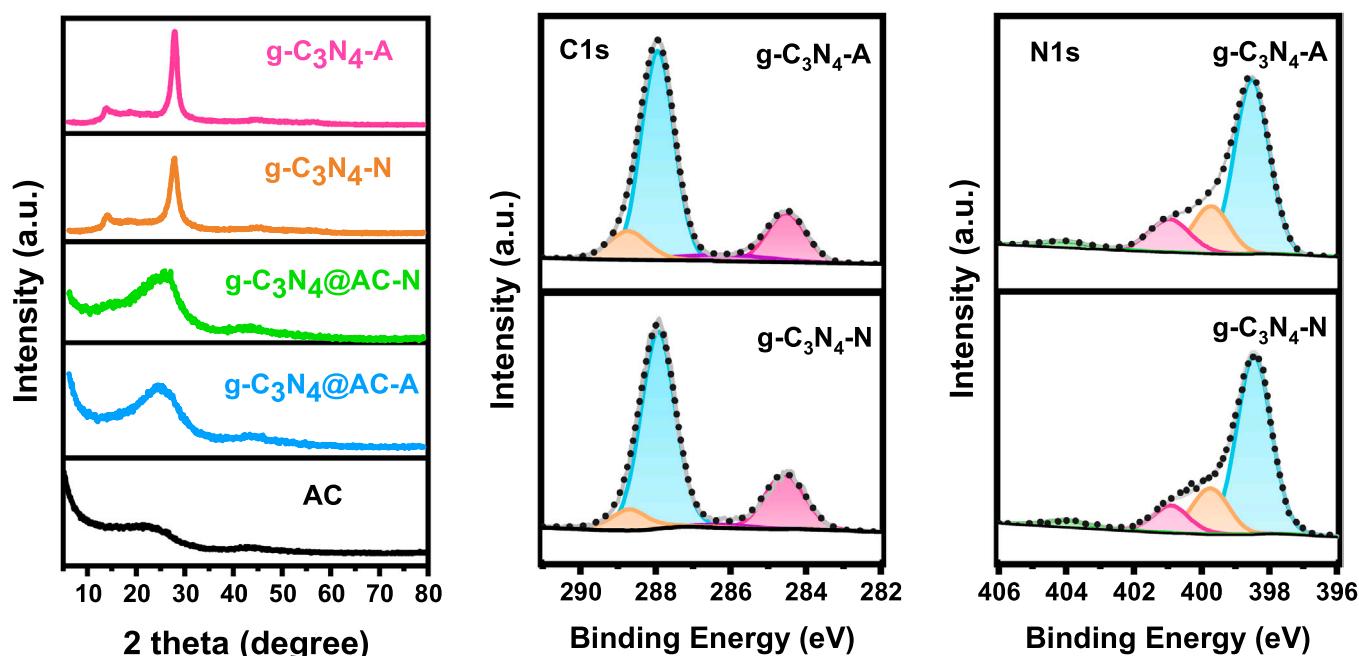


Fig. 2. XRD patterns of various catalyst samples and XPS spectra of pure g-C<sub>3</sub>N<sub>4</sub>-N and g-C<sub>3</sub>N<sub>4</sub>-A.

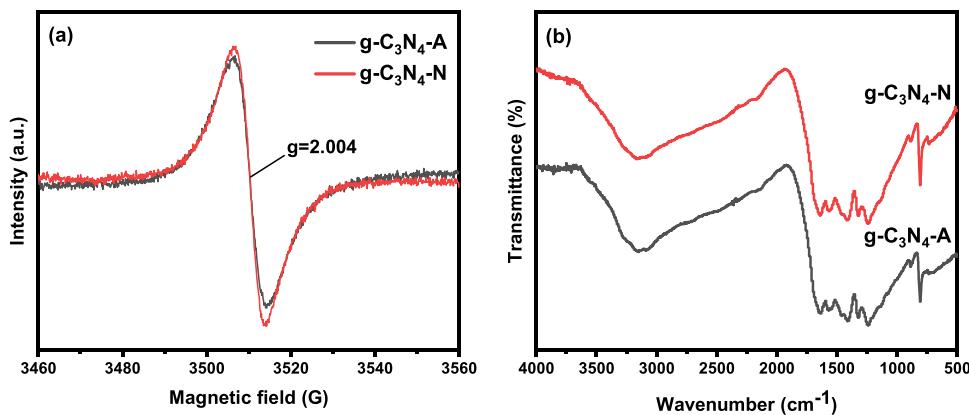


Fig. 3. (a) EPR and (b) FT-IR spectra of pure g-C<sub>3</sub>N<sub>4</sub>-N and g-C<sub>3</sub>N<sub>4</sub>-A samples.

determined by FT-IR spectra (Fig. 3b). The sharp peak at 808 cm<sup>-1</sup> of g-C<sub>3</sub>N<sub>4</sub>-A, assigned to the C-N stretching vibration of the characteristic tri-s-triazine structure, was weaker than that of g-C<sub>3</sub>N<sub>4</sub>-N (Fig. 3b), manifesting the appearance of more carbon vacancies since carbon vacancies destroyed the structural integrity of the tri-s-triazine structure [60,61]. In addition, FT-IR spectra in Fig. S2 showed that the main absorption peaks of g-C<sub>3</sub>N<sub>4</sub>-A and AC appeared in the spectra of g-C<sub>3</sub>N<sub>4</sub>@AC-A implying the interfacial interaction between g-C<sub>3</sub>N<sub>4</sub>-A and AC, which corresponded with XRD. This would induce the improvement of the catalytic efficiency.

Raman spectroscopy was a common method to characterize the defect of carbon materials. As we knew, the ratio of D band with G band ( $I_D/I_G$ ) was related with the defective content of carbon materials [62, 63]. It could see from the Raman spectra of g-C<sub>3</sub>N<sub>4</sub>@AC-N and g-C<sub>3</sub>N<sub>4</sub>@AC-A in Fig. 4 that the  $I_D/I_G$  value of g-C<sub>3</sub>N<sub>4</sub>@AC-A was bigger than that of g-C<sub>3</sub>N<sub>4</sub>@AC-N (5.33 vs 3.61), representing the more carbon defects in g-C<sub>3</sub>N<sub>4</sub>@AC-A.

As for the issue that the crystallite size from XRD did not support the activity test results for pure g-C<sub>3</sub>N<sub>4</sub>, we thought that the crystallite size was one of factors affecting catalytic activity and did not dominate the catalytic behavior. Taking the SEM, TEM, XRD, XPS, FT-IR, EPR and Raman spectrum together, it could be concluded that carbon defect in g-C<sub>3</sub>N<sub>4</sub> was responsible for the difference in the catalytic activity of g-C<sub>3</sub>N<sub>4</sub>-A and g-C<sub>3</sub>N<sub>4</sub>-N and air atmosphere more favored the formation of carbon defect.

Furthermore, the textural properties of various catalysts were investigated by N<sub>2</sub> adsorption-desorption method. As shown in Fig. 5,

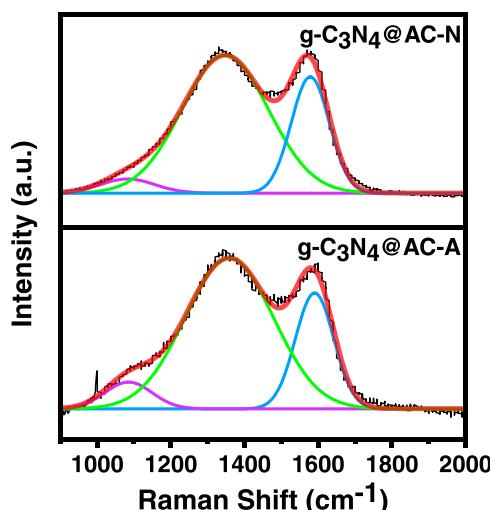


Fig. 4. Raman spectra of g-C<sub>3</sub>N<sub>4</sub>@AC-N and g-C<sub>3</sub>N<sub>4</sub>@AC-A.

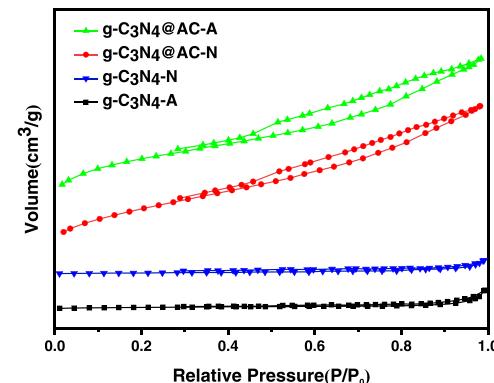


Fig. 5. N<sub>2</sub> adsorption/desorption isotherms of different catalyst samples.

the isotherms of all the samples displayed a type IV-like isotherm curve with hysteresis loop, indicative of mesoporous materials. Obviously, the supported g-C<sub>3</sub>N<sub>4</sub> catalysts possessed more developed pore system relative to pure g-C<sub>3</sub>N<sub>4</sub> catalysts (Table 3), which demonstrated that the support AC was able to well disperse g-C<sub>3</sub>N<sub>4</sub> (this was also supported by XRD characterization), thereby gaining the higher catalytic performance. And, the specific area and pore volume of g-C<sub>3</sub>N<sub>4</sub> @AC-A were much bigger than those of g-C<sub>3</sub>N<sub>4</sub> @AC-N. This suggested that the pyrolysis in air atmosphere could obtain more developed pore organization, which benefited catalytic performance.

### 3.3. The exploration of the universality of our procedure

With the optimized conditions in hand, the universality of our procedure was investigated using a wide range of structurally diverse nitrobenzenes and FA as starting materials. The results were summarized

Table 3

The textural properties of the as-prepared catalyst samples.

Sample	Specific surface area (m <sup>2</sup> /g)	Pore volume (cm <sup>3</sup> /g)	Mean pore size (nm)
g-C <sub>3</sub> N <sub>4</sub> -N	11.0	0.26	3.6
g-C <sub>3</sub> N <sub>4</sub> -A	11.4	0.35	4.0
g-C <sub>3</sub> N <sub>4</sub> @AC-N	275.6	0.30	4.0
g-C <sub>3</sub> N <sub>4</sub> @AC-A	499.6	0.40	4.1

According to the above analysis and appraisal, the high catalytic property of g-C<sub>3</sub>N<sub>4</sub> @AC-A could be ascribed to carbon defect and the dispersion effect of the support AC. Pyrolysis in air atmosphere obtained more carbon defects and the support AC effectively dispersed g-C<sub>3</sub>N<sub>4</sub> to expose more active sites.

**Table 4**

One-pot reductive formylation reactions of nitro compounds and FA catalyzed by g-C<sub>3</sub>N<sub>4</sub>@AC-A<sup>a</sup>.

Entry	Substrates	Reaction times (h)	1	5
			Yields of 5 (%) <sup>b</sup>	
1		10	98	
2		16	94	
3		14	94	
4		14	95	
5		14	99	
6		14	96	
7		14	98	
8		16	86	
9		16	72	
10 <sup>c</sup>		20	28	

<sup>a</sup>Reaction conditions: nitro compounds (5 mmol), FA (40 mmol), SF (10 mmol), g-C<sub>3</sub>N<sub>4</sub>@AC-A (0.3 g), 130 °C, N<sub>2</sub> atmosphere.

<sup>b</sup>GC Yields.

<sup>c</sup> Yield of N-(4-Formamidophenyl) formamide.

in Table 4. Overall, our protocol enabled the N-formylation of nitro aromatics containing both electron-donating (*-Me*, *-OMe*) and electron-withdrawing groups (*-F*, *-Cl*, and *-Br*) into the corresponding amides in good yields. The reactions of regioisomers of methylnitrobenzene with FA were investigated; a weak effect of steric hindrance was observed (Entry 3–5, Table 4). Moreover, dehalogenation was not found for halogenated nitrobenzenes, generally occurring in catalytic hydrogenation process. Aliphatic nitro compound nitropropane was also tested; its reactivity was noticeably lower than nitroarenes (Entry 9, Table 4). Additionally, for *p*-dinitrobenzene transformation, multiple products were formed based on GC-MS (such as *p*-nitroaniline, diphenylamine, *p*-aminobenzamide), only 28% yield of N-(4-Formamidophenyl) formamide was obtained under our given condition.

### 3.4. The reusability of the g-C<sub>3</sub>N<sub>4</sub>@AC-A catalyst

We explored the reusability of the g-C<sub>3</sub>N<sub>4</sub>@AC-A catalyst by the reductive formylation reaction of nitrobenzene and FA as the probe reaction. Prior to reuse in the next run, the catalyst needed to be washed using water and ethyl acetate orderly twice under ultrasound irradiation. The test reactions were performed under our optimized condition.

It could be seen from Fig. 6 that catalytic activity could be maintained during the first four rounds (from 98% to 95%) and a small activity loss was found in five rounds (90%); while we extended the reaction time to 12 h, a satisfactory yield was given (98%).

In order to explore the cause of recycled catalyst deactivation, we performed SEM, XRD, N<sub>2</sub> adsorption/ desorption, XPS and Raman spectroscopy characterization for the spent catalyst after 5 cycles (Fig. 7). SEM imagines of both the fresh and spent catalyst displayed numerous small particles on the substrate AC. No significant change was observed from SEM. XRD of the spent catalyst exhibited two broad peaks centered at 43.2° and 23.9°, which was similar to that of fresh catalyst. N<sub>2</sub> adsorption/desorption showed that the specific surface area and pore volume of the spent catalyst decreased compared to the fresh catalyst (seeing Fig. 7d). The main reason for this, we thought, was that reagent-(nitrobenzene, FA) and product (e.g. N-phenyl formamide) were adsorbed on the surface of catalyst, resulting in a decrease in the developed degree of pore organization. The full spectrum of XPS in Fig. 7e displayed that the content of N decreased and the content of O increased relative to the fresh catalyst after catalyst was reused, which supported the attachment of the reagent and product to the catalyst. Moreover, the I<sub>D</sub>/I<sub>G</sub> value from Raman spectrum decreased (from 5.33 of the fresh catalyst to 3.95 of the spent catalyst) (Fig. 7f), meaning the decrease of carbon defects in spent catalyst.

In a word, the cause of recycled catalyst deactivation should be that the attachment of the organics covered the active site, leading to the decline of catalytic performance according to above characterization.

To show the benefits and disadvantages of our procedure, we summarize the literature results for the reductive N-formylation of nitrobenzene. It can be seen in Table 5 that the advantage of our protocol is metal-free catalyst and solvent-free condition. g-C<sub>3</sub>N<sub>4</sub> @AC-A settles the high cost and metal leaching of metal catalyst. And, solvent-free reaction condition met the requirements of green chemistry. The catalytic performance and the universality for structurally diverse nitro compounds of our catalyst need to be improved. Thus, the following work is to further enhance catalytic performance of metal-free C-N composite and optimize reaction procedure to obtain the higher practicability.

### 4. Conclusion

An efficient, low cost and metal-free g-C<sub>3</sub>N<sub>4</sub>@AC-A catalyst was developed for one-pot reductive N-formylation of nitro compounds and sodium formate was introduced to speed up this reaction. Benefited of these, a broad set of nitro compounds were successfully converted to their corresponding formamides in good to high yields with various functional group tolerances under the solvent-free condition. Metal-free catalyst avoided the leaching of metal and metal pollution of product fundamentally. The catalyst could be recovered and recycled several times without marked loss of activity. Based on the instrument analyses, the high catalytic property of g-C<sub>3</sub>N<sub>4</sub>@AC-A could be ascribed to carbon

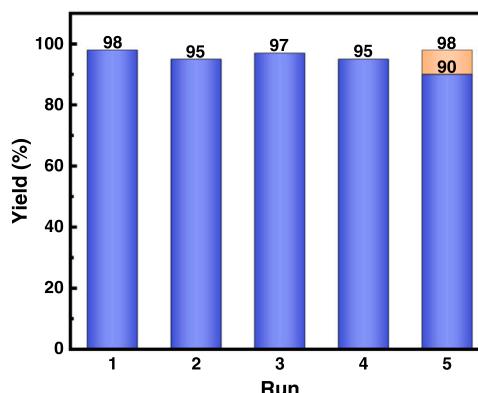
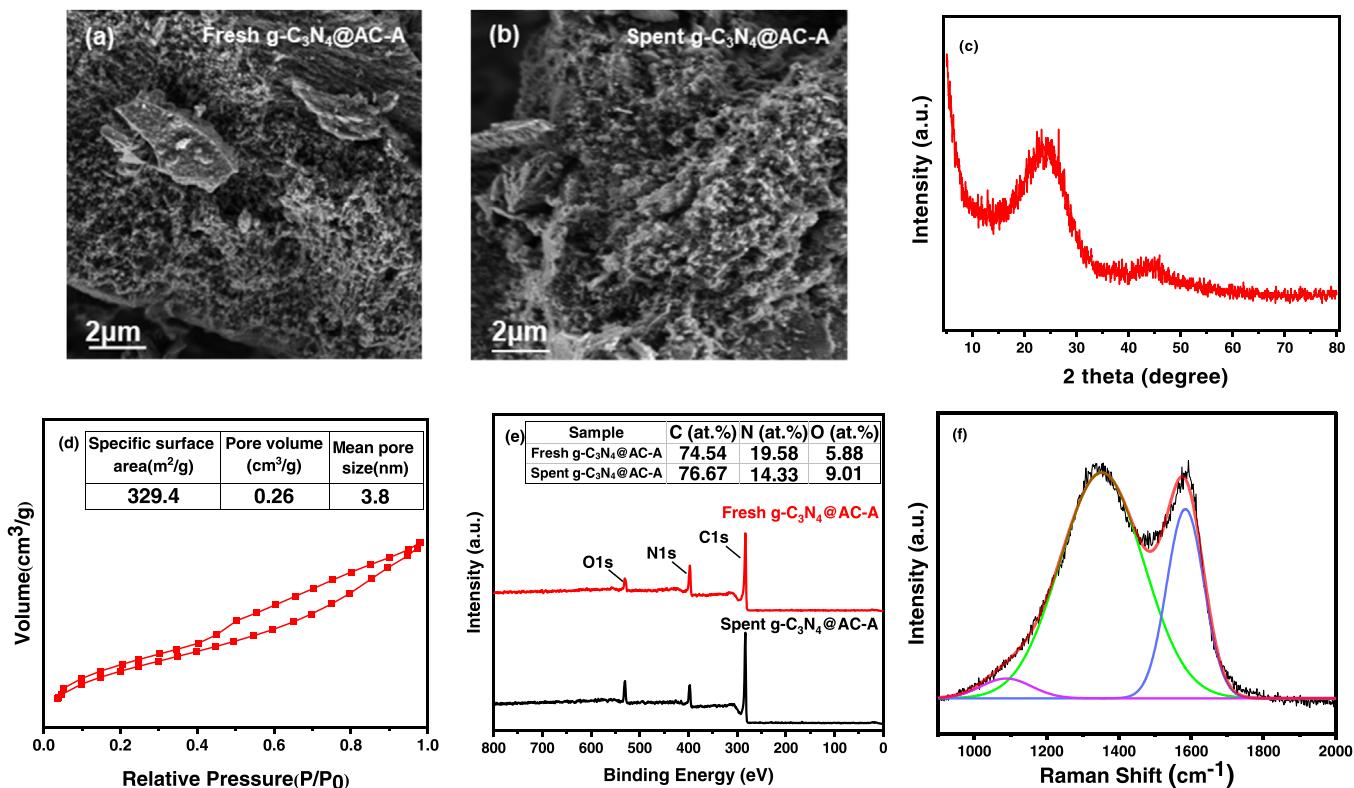


Fig. 6. Reusability of the g-C<sub>3</sub>N<sub>4</sub>@AC-A catalyst.

Fig. 7. SEM, XRD,  $\text{N}_2$  adsorption/desorption, XPS and Raman spectrum of spent  $\text{g-C}_3\text{N}_4@\text{AC-A}$  catalyst.

**Table 5**  
Comparison of various procedures for N- formylation of nitrobenzene.

Entry	Catalyst	Reaction condition	Yields (%)	References
1	AgPd@g- $\text{C}_3\text{N}_4$	Nitrobenzene (1 mmol); FA (2 mmol); catalyst (25 mg); water (1.0 mL); 40 watt domestic bulb; 2 h.	99	[16]
2	Au/rutile	Nitrobenzene (1 mmol); FA (4 mmol); Au (1 mol%); toluene(5 mL); $\text{N}_2$ (1 bar); 70 °C; 2 h.	96	[17]
3	Mag-IL-Pd	Nitrobenzene (0.25 mmol); FA (30equiv); catalyst (0.25 mol %); water (1 mL); Ar; 90 °C; 24 h.	97	[15]
4	CoNC-700	Nitrobenzene (0.5 mmol); FA (5 mmol); catalyst 9.5 mg (1 mol% Co); acetonitrile (5 mL); $\text{N}_2$ (1 bar); 110 °C; 6 h.	96	[19]
5	ZnNC-1000	Nitrobenzene (0.5 mmol); FA (6 equiv); catalyst(20 mg); THF (2 mL); Ar; 150 °C; 16 h.	96	[22]
6	ZnCo-N@C(ZIF-COF)	Nitrobenzene (1 mmol); FA (12 equiv); catalyst(30 mg); THF (7 mL); 200 °C; 8 h.	85	[21]
7	Co@NSC-800	Nitrobenzene (0.5 mmol); FA (14 equiv); catalyst (20 mg); water (3 mL); 110 °C; 5 h.	96	[20]
8	$[\text{Cp}^*\text{RhCl}_2]_2$	Nitrobenzene (1.6 mmol); FA (32 mmol); catalyst (0.1 mol %); KI(1.6 mmol); DMSO (2 mL); $\text{Et}_3\text{N}$ (10.7 mmol); Ar; 100 °C; 20 h	69	[18]
9	$\text{g-C}_3\text{N}_4@\text{AC-A}$	Nitrobenzene (5 mmol); FA (40 mmol), SF (10 mmol); catalyst (0.3 g); $\text{N}_2$ ;130 °C; 10 h.	98	This work

defect and the dispersion effect of the support AC. Air pyrolysis obtained more carbon defect and the support AC effectively dispersed  $\text{g-C}_3\text{N}_4$  and exposed more active sites. In summary, this study provided a green, efficient and practical methodology for the expedient synthesis of formamides from nitro compounds.

#### CRediT authorship contribution statement

Xing Wang: Validation, Formal analysis, Investigation, Data curation, Writing – original draft, Writing – review & editing. Xiaona Liu: Methodology, Validation, Data curation. Hui Wen: Validation, Formal analysis. Kai Guo: Formal analysis, Visualization. Hlomayi Brendon: Visualization, Writing – review & editing. Di Liu: Investigation, Conceptualization, Methodology, Resources, Supervision, Project administration, Funding acquisition, Writing – review & editing.

#### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

#### Data availability

Data will be made available on request.

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## Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.apcatb.2022.122042.

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